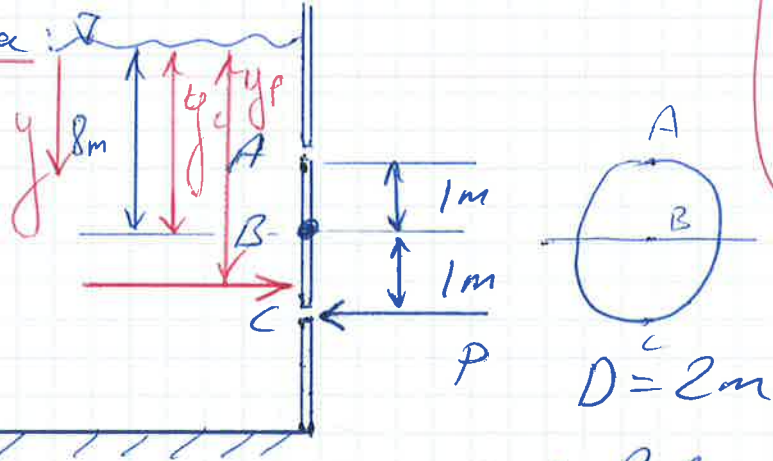


Q4 Known: Circular gate  
Find: a) hydrostatic force b) P to keep gate closed

Schematic + data:

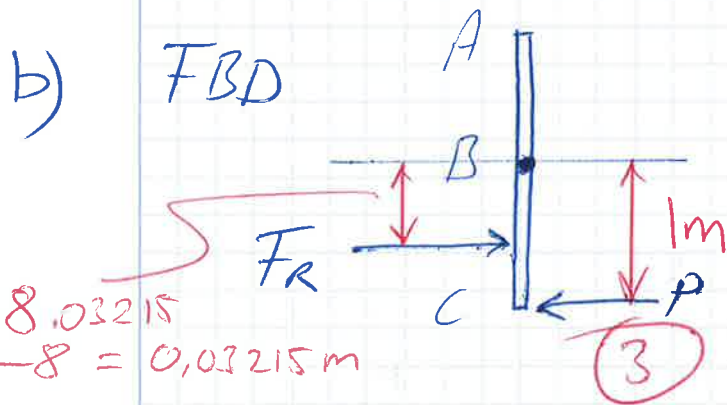
$$g = 9.81 \frac{m}{s^2} \downarrow$$

$$\rho = 10^3 \text{ kg/m}^3$$



a) Assume:  $\rho$  const., neglect weight, neglect  $P_{atm}$ .  
Analysis:  $F_R = P_c \cdot A$   
 $\Rightarrow F_R = \rho g y_c A$   
 $= 10^3 \frac{kg}{m^3} \cdot 9.81 \frac{m}{s^2} \cdot 8m \cdot \frac{\pi \cdot 2^2 m^2}{4} = 246.6 \text{ kN}$

$F_R$  is horizontal and acts @  $y_p = y_c + \frac{I_{xc}}{y_c A}$   
 $I_{xc} = \frac{\pi R^4}{4}$   
 $= 8m + \frac{\frac{\pi}{4} \cdot 1^4}{8m \cdot \frac{\pi \cdot 2^2}{4}}$   
 $= 8 + \frac{1}{4 \cdot 8}$   
 $= 8.03125m$



$\sum M_B = 0$   
 $\Rightarrow F_R (y_p - y_c) - 1m \cdot P = 0$

$\Rightarrow P = \frac{F_R (y_p - y_c)}{1m}$   
 $= \frac{246.6 \text{ kN} \cdot 0.03215m}{1m}$

point B is at  $y = 6/6$   $= 7.69 \text{ kN}$

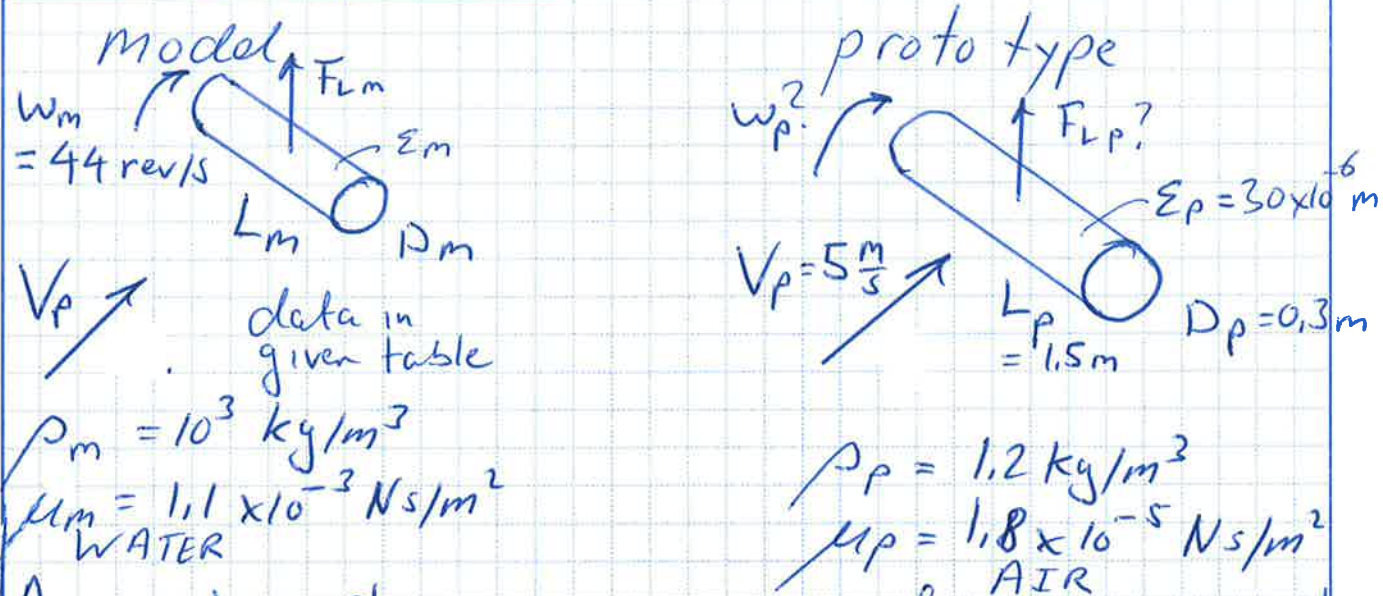
**THE UNIVERSITY OF ADELAIDE**  
**ENGINEERING DESIGN CALCULATIONS**

Date		Job No.	Sheet
Scale			
DRG-N BY		2/6	
Checked			

Q 5

Known: Rotating cylinder in a uniform flow  
find: a) dimensionless expression for  $F_L$   
 b) Compare prototype to which model?  
 c)  $\omega_p$   
 d)  $F_{Lp}$

Schematic + data:



Assumptions: Steady, incompressible flow, const properties. (1)

Analysis: list parameters, units and dimensions.

a)

parameter	units	dimension
$F_L$	N	$[MLT^{-2}]$
$L$	m	$[L]$
$D$	m	$[L]$
$\epsilon$	m	$[L]$
$\omega$	rev/s	$[T^{-1}]$
$V$	m/s	$[LT^{-1}]$
$\rho$	$\text{kg/m}^3$	$[ML^{-3}]$
$\mu$	$\text{N s/m}^2$	$[ML^{-1}T^{-1}]$

$n = 8$  parameters

$m = 3$  dimensions.

(2)

**THE UNIVERSITY OF ADELAIDE**  
**ENGINEERING DESIGN CALCULATIONS**

Date		Job No.	Sheet
Scale			
DRG-N BY			
Checked			

3/6

$n=8$  parameters,  $m=3$  dimensions.  $\Rightarrow$  need  $8-3=5$

$\Pi_1$ :  $L$  and  $D$  both have dimensions of  $[L] \Rightarrow \frac{L}{D} = \Pi_1$  (1)

$\Pi_2$ :  $\varepsilon$  and  $D$  both have dimensions of  $[L] \Rightarrow \Pi_2 = \frac{\varepsilon}{D}$

$\Pi_3$ : Viscous flow over body  $\Rightarrow$  use  $Re$   
 $\Rightarrow \Pi_3 = Re = \frac{\rho V D}{\mu}$  (or  $\frac{\rho V \varepsilon}{\mu}$  or  $\frac{\rho V L}{\mu}$ ) (3)

$\Pi_4$ : periodic rotation.  $\Rightarrow$  use  $St$   
 $\Pi_4 = St = \frac{\omega D}{V}$  (or  $\frac{\omega \varepsilon}{V}$  or  $\frac{\omega L}{V}$ )

$\Pi_5$ : Aerodynamic Lift force  $\Rightarrow C_L$   
 $C_L = \frac{F_L}{\frac{1}{2} \rho V^2 (LD)}$

$\leftarrow$  frontal Area. could be anything with units of  $m^2$ , but frontal area is most common.

$\Rightarrow \frac{F_L}{\frac{1}{2} \rho V^2 (LD)} = f\left(\frac{\rho V D}{\mu}, \frac{\omega D}{V}, \frac{L}{D}, \frac{\varepsilon}{D}\right)$

or  $C_L = f\left(Re, St, \frac{L}{D}, \frac{\varepsilon}{D}\right)$  (1)

**THE UNIVERSITY OF ADELAIDE**  
**ENGINEERING DESIGN CALCULATIONS**

Date		Job No.	Sheet
Scale			
DRG-N BY		4/6	
Checked			

b) For geometric similarity  $\frac{L}{D}|_m = \frac{L}{D}|_p$  and  $\frac{\Sigma}{D}|_m = \frac{\Sigma}{D}|_p$ .

$$\frac{L}{D}|_p = \frac{1.5}{0.3} = 5, \quad \frac{L}{D}|_{mA} = \frac{0.5}{0.1} = 5, \quad \frac{L}{D}|_{mB} = \frac{1}{0.2} = 5$$

$$\frac{\Sigma}{D}|_p = \frac{30 \times 10^{-6}}{0.3} = 10^{-5}, \quad \frac{\Sigma}{D}|_{mA} = \frac{1.0 \times 10^{-5}}{0.1} = 10^{-5}, \quad \frac{\Sigma}{D}|_{mB} = \frac{56 \times 10^{-6}}{0.2} = 28 \times 10^{-5}$$

⇒ The prototype is geometrically similar to model A. — ② or equivalent.

c) For kinematic similarity  $Re_m = Re_p$  and  $St_m = St_p$ . — ①

$$Re_m = Re_p \Rightarrow \frac{\rho V D}{\mu}|_m = \frac{\rho V D}{\mu}|_p$$

$$\Rightarrow V_m = \frac{\rho_p}{\rho_m} \cdot \frac{D_p}{D_m} \cdot \frac{\mu_m}{\mu_p} V_p$$

$$\Rightarrow \boxed{V_m = \frac{1.2}{10^3} \cdot \frac{0.3}{0.1} \cdot \frac{1.1 \times 10^{-3}}{1.8 \times 10^{-5}} \cdot 5 \frac{m}{s} = 1.1 \frac{m}{s}} \quad \text{--- ①}$$

$$St_m = St_p \Rightarrow \frac{\omega D}{V}|_m = \frac{\omega D}{V}|_p \Rightarrow \boxed{\omega_p = \frac{D_m}{D_p} \cdot \frac{V_p}{V_m} \cdot \omega_m}$$

$$= \frac{0.1}{0.3} \cdot \frac{5}{1.1} \cdot 44 \frac{\text{rev}}{s} = 66.7 \frac{\text{rev}}{s} \quad \text{--- ②}$$

d) when  $V_m = 1.1 \text{ m/s}$ ,  $F_{Lm} = 12.1 \text{ N}$   
as  $L/D|_m = L/D|_p$  &  $\frac{\Sigma}{D}|_m = \frac{\Sigma}{D}|_p$  &  $Re_m = Re_p$  &  $St_m = St_p$

$$\Rightarrow C_{Lm} = C_{Lp} \Rightarrow \frac{F_L}{\frac{1}{2} \rho V^2 L D}|_m = \frac{F_L}{\frac{1}{2} \rho V^2 L D}|_p \quad \text{--- ②}$$

$$\Rightarrow \boxed{F_{Lp} = \frac{\rho_p}{\rho_m} \left(\frac{V_p}{V_m}\right)^2 \cdot \frac{L_p}{L_m} \cdot \frac{D_p}{D_m} \cdot F_{Lm} = \frac{1.2}{10^3} \left(\frac{5}{1.1}\right)^2 \cdot \frac{1.5}{0.5} \cdot \frac{0.3}{0.1} \cdot 12.1 \text{ N}}$$

$$= 2.7 \text{ N} \quad \text{--- ②}$$

**THE UNIVERSITY OF ADELAIDE**  
**ENGINEERING DESIGN CALCULATIONS**

Date:		Job No.	Sheet
Scale			
DRG-N BY		5/6	
Checked			

Q6  
a)

Known: Centrifugal pump

find: Power to drive pump.

sch + data:  $\omega = 1200 \text{ rev/min}$

$$r_1 = 60 \text{ mm} \quad r_2 = 100 \text{ mm}$$

$$b = b_1 = b_2 = 20 \text{ mm}$$

$$\beta_2 = 55^\circ$$

$$V_1 = V_{f1} = 3.8 \text{ m/s}$$

$$\rho_{\text{H}_2\text{O}} = 10^3 \text{ kg/m}^3$$

Assumptions: ideal, incomp., steady, radial flow, 1-D.

Analysis:  $P = \dot{m} u_2 (u_2 - V_{f2} \cot \beta_2)$  — (1)

$$u_2 = r_2 \omega = 0.1 \text{ m} \cdot 1200 \frac{\text{rev}}{\text{min}} \cdot \frac{1 \text{ min}}{60 \text{ s}} \cdot \frac{2\pi \text{ rad}}{\text{rev}} = 12.56 \text{ m/s}$$

$$\dot{m} = \rho 2\pi r_1 b_1 V_{f1} = 10^3 \frac{\text{kg}}{\text{m}^3} \cdot 2\pi \cdot 0.06 \text{ m} \cdot 0.02 \text{ m} \cdot 3.8 \frac{\text{m}}{\text{s}} = 28.65 \text{ kg/s}$$

from continuity

$$\dot{m}_{in} = \dot{m}_{out} \Rightarrow \cancel{\rho 2\pi r_1 b_1 V_{f1}} = \cancel{\rho 2\pi r_2 b_2 V_{f2}} \Rightarrow V_{f2} = \frac{r_1}{r_2} V_{f1} = \frac{0.06}{0.1} \cdot 3.8 = 2.28 \frac{\text{m}}{\text{s}}$$

$$\text{eqn (1)} \Rightarrow P = \dot{m} u_2 (u_2 - V_{f2} \cot \beta_2) = 28.65 \frac{\text{kg}}{\text{s}} \cdot 12.56 \frac{\text{m}}{\text{s}} \cdot \left[ 12.56 \frac{\text{m}}{\text{s}} - 2.28 \cot 55^\circ \right]$$

$$= 2488 \frac{\text{kg}}{\text{s}} \frac{\text{m}^2}{\text{s}^2}$$

$$\approx 2.5 \text{ kW}$$

(2)

15

Q6  
b) All are derived from Reynolds Transport Theorem. 2

c) Newtons 2<sup>nd</sup> Law of motion  $\vec{\Sigma F} = m \cdot \vec{a}$   
The N-S eqn accounts for viscous forces, the Euler eqn does not. 2  
1

2  
/2  
3  
20

Q4  
b) i)  $y_p = y_c + \frac{I_{xc}}{y_c A}$

so as  $y_c \rightarrow \infty$ ,  $y_p \rightarrow y_c$  2  
 $y_p$  &  $y_c$  get closer together

ii)

intensive  
Specific vol  
density  
concentration  
temp,  $\mu$   
viscosity

extensive  
Volume  
Momentum

"not a property"  
heat transfer

2